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## In vitro hydrogen photoproduction using *Pyrococcus furiosus* sulfhydrogenase and TiO<sub>2</sub>

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#### Abstract

The [NiFe] sulfhydrogenase from the hyperthermophilic archaeon *Pyrococcus furiosus* has been tested as a biological catalyst in a lightdriven in vitro hydrogen evolution system, using a solar simulator apparatus as a source of light. The enzyme is active when coupled to photo-induced titanium dioxide (TiO<sub>2</sub>) dispersed as submicronic powder in a buffer solution and in the presence of the artificial redox mediator methylviologen (MV), carrying electrons from the TiO<sub>2</sub> particle to the enzyme. To optimize the system towards practical applications, a simplified version which works in the absence of MV was set up and its performance was assayed with different reductants, as a function of time and over a wide range of temperatures. The comparison of MV-mediated and not-mediated conditions in terms of rate and amount of H<sub>2</sub> photoproduced, highlights a lower efficiency, but an improved overall stability of the system when a direct electron transfer from the TiO<sub>2</sub> to the enzyme takes place. As a consequence, the reaction lifetime is productively extended counteracting the effect of the low H<sub>2</sub> evolution rate with regard to the total amount of H<sub>2</sub> photoproduced. In particular, at 60°C the reaction lifetime is prolonged to 8 h, thus resulting in significantly higher amount of H<sub>2</sub> evolved. The flexibility of the *P. furiosus* sulfhydrogenase/TiO<sub>2</sub> in vitro system with respect to the redox mediator MV and the evidence that the enzyme performance can be maintained over a wide range of temperatures (60– 80°C) are promising advances in the identification of the optimal conditions for the development of an economically feasible hydrogen production process exploiting solar light as a source of energy and waste compounds as electron donors. © 1999 Elsevier Science S.A. All rights reserved.

Keywords: Hydrogen photoproduction; P. furiosus sulfhydrogenase; Titanium dioxide; Methylviologen

### 1. Introduction

The basic requirement for hydrogen to be considered as an alternative energy source of the future is the development of economically feasible production systems, since its advantages as a fuel are generally acknowledged. It is, in fact, efficient, renewable and environmentally friendly, since its combustion does not generate toxic byproducts.

Among hydrogen production technologies, those based on biological systems represent an attractive possibility. Since the early 1970s, research efforts in the field of biohydrogen have been particularly addressed to biophotolysis and photofermentations, the latter combining hydrogen production to the disposal of waste compounds used as growth substrates [1]. Both strategies exploit sunlight as an energy source for microorganisms and are promising to make the bioproduction of hydrogen competitive with conventional systems, such as chemical and electrochemical methods [1].

Unlike in vivo technologies, light-driven in vitro enzymatic systems have been less considered as potential methods for biohydrogen production. Nevertheless, since the early 1980s different hydrogenases, the enzymes catalyzing the reaction  $2H^+ + 2e^- \Leftrightarrow H_2$ , have been successfully employed in photoevolution processes coupled with semiconductors and sensitizers in the presence of artificial or natural electron carriers [2-5]. Likewise, the principle of the photoreactivity of finely dispersed TiO<sub>2</sub> powder in aqueous solution is a well studied phenomenon and many applications, mostly associated with polluted water treatment, are described in the literature [6]. TiO<sub>2</sub> has also been employed in photoevolution experiments coupled to redox enzymes, such as hydrogenases, able to successfully replace inorganic catalysts [7,8] in the generation of molecular hydrogen [3-5]. Interestingly, the ability of the hydrogenases tested, all of them isolated from mesophilic organisms, to directly accept electrons from the light-excited semiconductor without the requirement of any redox mediator was also reported [9,10]. These early experiments pointed out some relevant problems

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of these in vitro systems that remain to be solved in view of possible practical applications, namely the cost of the catalyst, its instability and the limited lifetime of the reaction.

With regard to the instability of the enzymatic component, the use of hydrogenases from thermophilic or hyperthermophilic organisms might represent an advantage, since these enzymes exhibit biochemical and structural features particularly attractive for applicative purposes [11,12]. In fact, in addition to thermostability, they are endowed with high catalytic efficiency, oxygen tolerance and resistance to chemical and denaturing agents.

We previously reported on the performance of two thermotolerant enzymes, the hydrogenase from the eubacterium Acetomicrobium flavidum and the bifunctional sulfhydrogenase from the archaeon Pyrococcus furiosus, in an in vitro heterogeneous system in which H<sub>2</sub> is photocatalytically produced by coupling the biocatalysts to the light-induced finely dispersed semiconductor TiO<sub>2</sub> [13,14]. This early set up also included the presence of the artificial redox mediator methylviologen (MV) and was assayed at temperatures close to the optimum for each enzyme. In the experimental conditions used, the overall performance of the P. furiosus sulfhydrogenase proved to be superior to that of the A. flavidum enzyme and the direct utilization of electrons, available from the irradiated semiconductor, could be demonstrated only in the case of the archaeal protein [14]. P. furiosus sulfhydrogenase was also successfully employed by others in a different in vitro system for the generation of molecular H2 based on the oxidation of glucose and in combination with the glucose dehydrogenase from Thermoplasma acidophilum [15].

These experimental data brought us to the conclusion that the *P. furiosus* enzyme is of particular interest for further investigations aimed at establishing the optimal conditions for practical applications of the light-driven in vitro system coupled to TiO<sub>2</sub>. *P. furiosus* sulfhydrogenase is a bifunctional enzyme the physiological role of which, depending on growth conditions is either proton reduction to H<sub>2</sub> or sulphur species reduction to H<sub>2</sub>S [16]. Its bifunctionality is probably based on the presence of two structurally different components which are assembled as a tetramer ( $\alpha\beta\gamma\delta$ ) in the native conformation [17]. Its physiological electron donor is NADPH [18] and this is very unusual, since only a few hydrogenases are able to utilize nicotinamide nucleotides as electron carriers.

Three critical points of the MV-mediated *P. furiosus* sulfhydrogenase/TiO<sub>2</sub> system, as far as the reaction kinetics is concerned, were identified [13,14]: (i) H<sub>2</sub> photoproduction is a high-rate but a short-term reaction; (ii) the presence of MV, carrying electrons from the irradiated TiO<sub>2</sub> particle to the biocatalyst, enhances the H<sub>2</sub> evolution rate but strongly affects the lifetime of the reaction, since it undergoes irreversible degradation; (iii) Tris, used as a buffer, proved to be an efficient electron donor for TiO<sub>2</sub>, but its oxidation affects the stability of the system since under these condi-

tions the pH changes in the course of the reaction. Alternative and possibly renewable compounds would be preferable as a source of electrons, particularly in view of a scaling-up.

These results prompted us to further investigate the performance of the *P. furiosus* sulfhydrogenase/TiO<sub>2</sub> system in the absence of MV as a first optimization step towards its practical application for biohydrogen production.

The present report deals with the setting up of a simplified system which includes only three reaction components: the inorganic semiconductor, the biological catalyst and the buffer. In particular, we describe the functional scheme of the not-mediated *P. furiosus* sulfhydrogenase/TiO<sub>2</sub> in vitro system and a comparative evaluation of its performance, in terms of rate and amount of H<sub>2</sub> produced, with respect to the mediated system in different experimental conditions.

### 2. Experimental

#### 2.1. Chemicals

 $TiO_2$  powder (50 m<sup>2</sup>/g) was purchased from Degussa. Sodium dithionite, methyl viologen dichloride and Tris (tris(hydroxymethyl)aminomethane) were purchased from Fluka. Chromatographic media and columns were from Pharmacia. The other chemicals used were of the purest grade available commercially.

### 2.2. P. furiosus growth and sulfhydrogenase purification

*P. furiosus* (DSM3638) was cultured and its sulfhydrogenase was partially purified according to the procedures previously reported [19,20]. Hydrogenase activity was colorimetrically visualized after each chromatographic step by SDS-PAGE analysis [19]. Finally, the hydrogenase-containing fractions were diluted in 50 mM Tris-HCl pH 8 buffer at a protein concentration of about 3 mg/ml, as estimated by the Bio-Rad micromethod based on the Bradford assay [21]. The purity degree of the enzyme, as judged by SDS-PAGE analysis, was about 10% with a specific activity of 10.8 U/ mg.

#### 2.3. Hydrogenase activity assay

Hydrogenase activity was measured anaerobically at  $80^{\circ}$ C in 12 ml deaerated vials containing 50 mM Tris-HCl at pH 8, 1 mM methylviologen and 25 mM sodium dithionite (Na<sub>2</sub>S<sub>2</sub>O<sub>4</sub>) as an electron donor. Reaction mixtures contained approximately 0.6 mg of sulfhydrogenase in 5 ml buffered solution. One unit is defined as the amount of enzyme which produces 1  $\mu$ M of hydrogen per minute.

Hydrogen production was determined by gas chromatography on a Varian 3400 instrument equipped with a 5 Å MolSieve column ( $6' \times 1/8''$ ) and Thermoconductivity detector. Carrier gas was Ar at a flow rate of 30 ml/min. Usually, 0.2 ml of the gas phase present in the headspace of the reaction vial were injected at regular intervals.

#### 2.4. Solar box experiments

Hydrogen photoproduction experiments were performed in an AM1 solar simulator box equipped with a Xenon lamp (1500 W/m<sup>2</sup>) produced by CO.FO.ME.GRA, Italy. The photometric measurement of the irradiation inside the box (15 cm from the light source) was approximately 120 klux. Kinetic experiments with the *P. furiosus* sulfhydrogenase were performed at different temperatures in jacketed pyrex glass vials (14 ml, total volume) closed by a tight-fitting rubber stopper and under magnetic stirring to homogenize the photoinduction of the white colloidal suspension.

Typically, in not-mediated experiments, the reaction mixture (5 ml) contained: 50 mM Tris-HCl buffer solution at pH 8, 20 mg TiO<sub>2</sub>, 0.2 ml of *P. furiosus* sulfhydrogenase (6.6 U). In mediated conditions, 1 mM MV was also added.

#### 3. Results and discussion

The reaction scheme of the system set up for initial evaluation tests on *P. furiosus* sulfhydrogenase included MV as an artificial redox mediator and Tris as an electron donor (sacrificial) [13,14]. The electron transfer pathway among the different components in the mediated condition (A) is shown in Fig. 1.

Provided that the biological catalyst is in the redox active state, hydrogen evolution occurs, under light irradiation, as a continuous electron flow from the donor Tris to protons, with MV carrying electrons accumulated on the  $TiO_2$  particle to the enzyme.

The electron transfer pathway in not-mediated conditions (B) is also illustrated in Fig. 1. Without the mediation of the

electron carrier, the enzyme is directly reduced at the  $TiO_2$  surface and electrons are transferred from the light-excited semiconductor to the biological catalyst. On the basis of previous results, a decrease in the rate of  $H_2$  evolution in notmediated conditions can be predicted as a result of the MV exclusion [13]. However, from an applicative point of view, the negative effect in terms of efficiency is balanced by a higher overall stability of the system components, which maximize the lifetime of the reaction and by the economical benefit related to the cost of MV.

# 3.1. $H_2$ evolution by P. furiosus sulfhydrogenase in mediator-independent conditions

The effect of the absence of the redox mediator MV on the kinetics of in vitro H<sub>2</sub> evolution by *P. furiosus* sulfhydrogenase was first evaluated by comparing the performance of the enzyme at  $80^{\circ}$ C using either sodium dithionite (Na<sub>2</sub>S<sub>2</sub>O<sub>4</sub>) or photoinduced TiO<sub>2</sub> as a reductant in mediated and not-mediated conditions. Sodium dithionite is typically used as an electron donor in standard evolution assays of hydrogenase enzymes.

Table 1 shows the results obtained, as far as initial rates and amounts of  $H_2$  evolved after 1 hour of reaction are concerned. As expected, in mediated conditions *P. furiosus* sulfhydrogenase is more efficient when coupled to Na<sub>2</sub>S<sub>2</sub>O<sub>4</sub> than when combined to the light-excited semiconductor TiO<sub>2</sub>: both the initial rate and the total amount of hydrogen evolved are about 3.5 times higher in the former than in the latter system. In fact, the formation of reduced MV by Na<sub>2</sub>S<sub>2</sub>O<sub>4</sub> does not represent a rate limiting step and therefore hydrogen evolution is mainly dependent on the enzyme activity. On the other hand, using photoinduced TiO<sub>2</sub>, the reaction kinetics is mostly dependent on the fraction of enzyme productively adsorbed on the TiO<sub>2</sub> surface.



Fig. 1. In vitro  $H_2$  photoproduction system based on *P. furiosus* sulfhydrogenase coupled to the semiconductor  $TiO_2$ : scheme of the electron transfer pathway in the presence (mediated, A) and in the absence (not-mediated, B) of the artificial redox mediator MV. Tris is the electron donor (sacrificial).

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Experimental condition	Initial rate of $H_2$ evolution (µmoles/min/mg)	$H_2$ amount after 1 h of reaction (µmoles)
Na <sub>2</sub> S <sub>2</sub> O <sub>4</sub> /MV (mediated)	11	145
$Na_2S_2O_4$ (not-mediated)	1.7	48
hv/TiO <sub>2</sub> /MV (mediated)	3.1	41
$hv/TiO_2$ (not-mediated)	1.3	29

Experiments were carried out at  $80^{\circ}$ C using 0.12 mg/ml of semipurified *P. furiosus* sulfhydrogenase. Hydrogen evolution was measured gaschromatographically. Concentrations of other reagents were: 25 mM Na<sub>2</sub>S<sub>2</sub>O<sub>4</sub>, 4 mg/ml TiO<sub>2</sub>, 50 mM Tris-HCl at pH 8 and 1 mM MV in the case of mediated conditions.

Without the mediation of MV,  $H_2$  evolution was measured in both in vitro systems. This might suggest that the ability of directly accepting electrons from either Na<sub>2</sub>S<sub>2</sub>O<sub>4</sub> and TiO<sub>2</sub> is an intrinsic property of the *P. furiosus* sulfhydrogenase, probably based on the presence of the two additional subunits which are also likely to be involved in electron transfer.

As far as initial rates are concerned, the effect of the absence of the redox mediator MV is more significant using  $Na_2S_2O_4$  as a reductant, being the value about 6.5 times lower than in mediated condition, whereas only a 2.4 fold decrease is measured using photoinduced TiO<sub>2</sub>.

With regard to the amounts of gas obtained after 1 h of reaction, again the performance of the light-driven  $TiO_2$  system is less dependent on the presence of MV, since the micromoles of hydrogen evolved in not-mediated condition are only 1.4 times less than in mediated condition, while a 3-fold decrease is measured using Na<sub>2</sub>S<sub>2</sub>O<sub>4</sub> as a reductant.

Therefore, the experimental data point out that the in vitro system combining *P. furiosus* sulfhydrogenase to photoinduced  $TiO_2$  is quite flexible with respect to the presence or absence of the artificial redox mediator MV, allowing its exclusion from the reaction without a dramatic loss in terms of rate and amount of hydrogen production. It is worth noting that with both reductants, the total amount of hydrogen evolved is less affected than the initial rate by the absence of MV. This is particularly true in the case of  $TiO_2$ -dependent heterogeneous photocatalysis, suggesting a different time-course of the reaction in mediated and not-mediated conditions.

# 3.2. Time-course of $H_2$ photoproduction in mediated and not-mediated conditions

The performance of the light-driven *P. furiosus* sulfhydrogenase/TiO<sub>2</sub> system in mediated and not-mediated conditions was then evaluated as a function of the reaction time. The time-course patterns of the rate and of the amount of hydrogen photoproduced at 80°C in mediated and notmediated conditions are shown in Fig. 2(A) and (B), respectively. In the presence of MV, the rate of hydrogen evolution is high during the first 30 min and, as already pointed out, the initial value is about 2.4 times higher than in not-mediated condition (Fig. 2(A)). Afterwards, it rapidly decreases and within 1 h of reaction time it is close to zero. Values of hydrogen evolution rate remain low during the two additional hours of reaction, indicating that, under these experi-



Fig. 2. Time-course of the rate (A) and the amount (B) of hydrogen photoproduced by *P. furiosus* sulfhydrogenase coupled to  $TiO_2$  at 80°C in mediated and in not-mediated conditions.

mental conditions, the *P. furiosus* sulfhydrogenase/ $TiO_2$  system is no longer active. After 3 h of reaction, the total amount of hydrogen evolved in mediated condition is about 47 mM, mostly as a result of the first hour of photoproduction (Fig. 2(B)). After that time, in fact, the hydrogen evolution reaches the plateau.

On the other hand, in the absence of MV the initial rate is rather low, but more constant and values close to zero are measured only after 3 h of reaction. As a consequence, the hydrogen evolution is productively extended and the plateau is reached later than in the presence of MV, thus giving rise to a similar amount of gas (about 52 mM).

In conclusion, the evaluation of the time-dependent performance of the light-driven *P. furiosus* sulfhydrogenase/  $TiO_2$  system in mediated and not-mediated conditions indicates that when a direct electron transfer takes place the system is less efficient as a lower H<sub>2</sub> evolution rate is obtained, but since the system gains in stability, the reaction lifetime is prolonged and the total amount of gas produced is similar to that obtained in MV-mediated condition. Therefore, for its overall performance and for its improved economics, the not-mediated *P. furiosus* sulfhydrogenase/TiO<sub>2</sub> system can successfully replace the early set up in view of practical applications in H<sub>2</sub> photoproduction.

# 3.3. Temperature-dependent $H_2$ photoproduction in mediated and not-mediated conditions

Another fundamental aspect to be considered for applicative purposes is the performance of the invitro system as a function of temperature. In fact, besides economical benefits, temperatures lower than 80°C could be helpful to improve the thermochemical stability of the reaction components and therefore might have a further positive effect on the lifetime of the reaction. The flexibility of the system as a function of temperature will depend on the thermophilicity of the biological catalyst. This determines in fact, the range of temperatures within which the *P. furiosus* sulfhy-drogenase/TiO<sub>2</sub> couple is functionally active in  $H_2$  photoproduction.

The performance of mediated and not-mediated systems at different temperatures was evaluated in terms of total amount of  $H_2$  evolved and duration of the reaction. In Fig. 3, the results obtained are reported.

As a general effect of lowering the reaction temperature below  $80^{\circ}$ C, a significative extension of the H<sub>2</sub> photoevolution lifetime is obtained both in mediated and not-mediated condition. On the other hand, at 90°C the performance of the in vitro system is clearly compromised, especially in terms of gas production, independently from the presence or the absence of the redox mediator MV.

At temperatures lower than  $80^{\circ}$ C in mediated condition, the prolonged lifetime of the reaction does not correspond to a remarkable increase in H<sub>2</sub> evolution due to the irreversible degradation of the redox mediator MV from the first hour reaction on. On the other hand, with the not-mediated system run in the same temperature conditions, the extension of the reaction lifetime is coupled to a significantly higher amount of gas evolved down to 50°C, which therefore represents the lower temperature limit for the thermophilic sulfhydrogenase to be active. The temperature range included between  $60^{\circ}$  and  $70^{\circ}$ C thus represents the best compromise between the thermophilicity of the enzyme and the thermochemical stability of the reaction components.

Particularly promising are the results obtained in notmediated condition at  $60^{\circ}$ C, the temperature which gives rise to an extension of the reaction lifetime from 5 to 8 h and to the highest amount of H<sub>2</sub> evolved (Fig. 3(A)). Although  $60^{\circ}$ C does not represent the optimum temperature as far as the initial rate is concerned, being about 2.6 times lower than at  $80^{\circ}$ C, the values remain stable over a longer period of time, leading to a 1.8 fold increase of H<sub>2</sub> photoproduced with respect to the same condition at  $80^{\circ}$ C and to a 1.6 fold



Fig. 3. Time-course of the amount of hydrogen photoproduced by *P. furiosus* sulfhydrogenase coupled to  $TiO_2$  at different temperatures in not-mediated (A) and in mediated conditions (B). Reaction lifetimes correspond to the period of active H<sub>2</sub> photoproduction.

increase when compared to the mediated system run at the same temperature.

In conclusion, the not-mediated *P. furiosus* sulfhydrogenase/TiO<sub>2</sub> system represents a first optimization step towards the development of an economically feasible in vitro hydrogen production process which should be driven by solar light and should utilize waste compounds as source of electrons. The present version, in fact, shows the following advantages compared to the mediator-dependent approach: (i) a simpler and more inexpensive experimental set up, including only three components (the inorganic semiconductor, the biological catalyst and the buffer) instead of four; (ii) an improved overall stability, which allows the lifetime of H<sub>2</sub> evolution to be productively extended and (iii) a better performance at lower temperatures, since the extension of the reaction lifetime is coupled to a significantly higher amount of H<sub>2</sub> photoproduced.

It is also worth mentioning some advantages related to the use of the *P. furiosus* sulfhydrogenase as a biological catalyst. The evidence that a minimal degree of purification is required for the enzyme to be employed in the in vitro system represents another advantage from an economical point of view, since its purification procedure is a particularly complex and expensive multi-step operation. In addition, its stability as a biological catalyst and its versatility in terms of reaction temperatures ( $60-80^{\circ}$ C) represents a further evidence of the biotechnological potential of this enzyme.

Future investigations will be addressed to optimize another critical point of the system which concerns the use of Tris and its dual role as a buffer and as an electron donor for TiO<sub>2</sub>. Alternative and renewable electron donors will be tested in mediator-independent condition. The screening of sacrificials different from Tris will be also performed with the aim of improving the oxidative transfer rate at TiO<sub>2</sub> surface. The photo-oxidation process, in fact, represents a fundamental issue as far as the efficiency of the system is concerned. As already pointed out, the use of waste products as source of electrons will be considered mainly because their disposal, coupled to H<sub>2</sub> photoproduction, would allow lower costs of process realization and management, besides making the system environmentally attractive.

The replacement of Tris with waste products will cause the absence of a buffering system to become the critical factor and the possibility of developing an on-line pH control system will be considered.

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